

Electrochemical Method for Monitoring Corrosive Impurities in Molten $\text{MgCl}_2/\text{KCl}/\text{NaCl}$ Salts for Thermal Energy Storage

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INTRODUCTION

- **Molten chloride salt mixtures** are promising thermal energy storage (TES) materials in **concentrated solar power (CSP)** plants due to physicochemical and thermal properties, e.g., **High thermal stability** (up to 700 °C) for higher efficiency of thermal to electrical energy conversion.
- However, the application of molten chloride salts at higher temperatures causes additional challenges, particularly **increased corrosiveness** of structural materials.
- Corrosion rates significantly depend on concentration of **oxide/hydroxide impurities** in the molten salts [1-3].
- In this work, an electrochemical analysis system based on **cyclic voltammetry (CV)** is being developed to measure the concentration of impurities in molten salts *in-situ* for **corrosion control**.



METHODS

Set-up for CV tests

- Tungsten as working electrode to *in-situ* measure concentration of MgOH^+
- Glassy carbon as working electrode for O^{2-}
- Salt sample collector for salt sample collection
- Acid consumption method (AC) for post-analysis of impurities concentration in salt samples

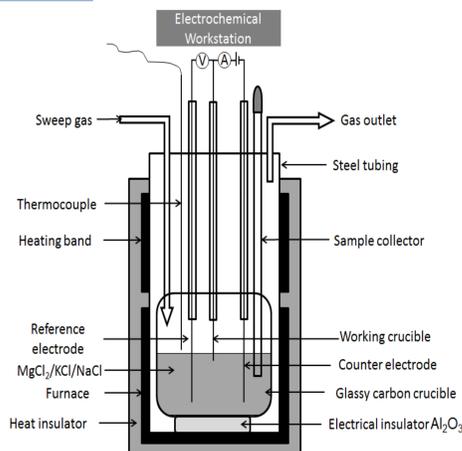


Figure 1: Schematic of experimental set-up for CV experiments on molten salts $\text{MgCl}_2/\text{KCl}/\text{NaCl}$ (60/20/20 mole%). Counter and reference electrodes are both tungsten.

Cyclic voltammetry (CV)

- Electrochemical reactions in Figure 2 [4]:
A: $\text{Mg}^{2+} + 2\text{e}^- = \text{Mg}$
A': $\text{Mg} = \text{Mg}^{2+} + 2\text{e}^-$
B: $\text{MgOH}^+ + \text{e}^- = \text{MgO} + \frac{1}{2} \text{H}_2$
C: $\text{Cl}^- = \frac{1}{2} \text{Cl}_2 + \text{e}^-$
- Relation between peak current density i_p and bulk concentration c^∞ of reactive species, e.g. [4]:

$$i_p(B) = k(T, \nu) \cdot c^\infty(\text{MgOH}^+)$$

$k(T, \nu)$: Constant as a function of temperature T and sweep rate ν .

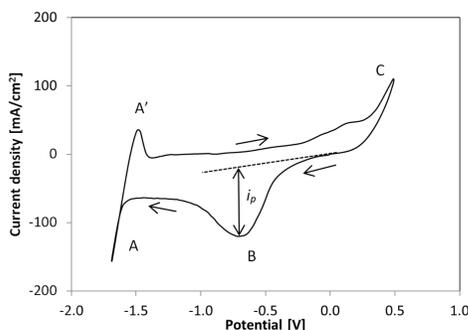


Figure 2: Cyclic voltammogram obtained on a tungsten electrode in the eutectic $\text{MgCl}_2/\text{KCl}/\text{NaCl}$ at 500 °C. Sweep rate ν : 200 mV/s. Counter and reference electrodes are both tungsten.

ACKNOWLEDGMENTS

This research is funded by DAAD and DLR within the DLR-DAAD postdoc fellowship programme.

RESULTS

Pre-electrolysis (PE)

- Direct current PE
- Voltage between the working and counter electrode = -2V
- Remove of the noise in cyclic voltammograms caused by unknown impurities

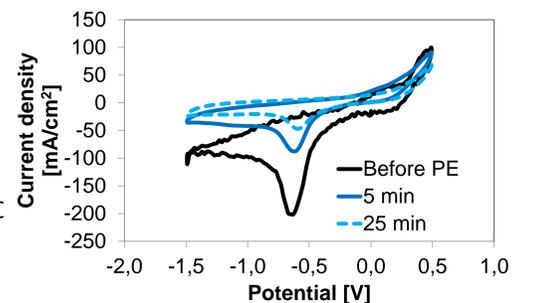


Figure 3: Cyclic voltammograms of molten salts before and after direct current pre-electrolysis at 500 °C. Working, counter and reference electrodes are tungsten. Sweep rate: 200 mV/s.

Determination of $k(T, \nu)$ from PE data

- Fitting concentrations of MgOH^+ from CV with those from AC via the least-square method:
$$\sum_{i=1}^n (c_i^{CV}(k) - c_i^{AC})^2 = \text{minimal}$$
- $k(T, \nu) = 1.8 \pm 0.6 \text{ A m/mol}$

CV experiments after adding NaOH

- Confirmation of Peak B for MgOH^+ : a significant change of peak B was observed after adding NaOH.
- The concentrations of MgOH^+ determined from AC compare well with those from the CV experiments, when the determined constant $k(T, \nu)$ from PE was used in the calculation.

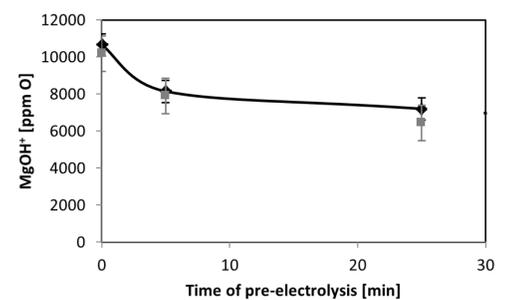


Figure 4: Concentrations of corrosive impurity MgOH^+ in molten salt over the time of PE determined with the CV (black curve) and acid consumption (grey points) method, respectively.

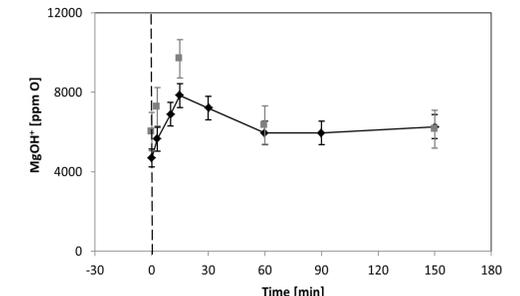


Figure 5: Concentration of MgOH^+ (black points and curve: CV data; Grey points: AC data) as a function of time after adding 4286 ppm O NaOH.

CONCLUSIONS & APPLICABILITY

This work presented the successful commissioning of an experimental set-up to study molten chloride melts *in-situ* (by CV) and *ex-situ* (post-analysis of salt samples by AC). Correlation between both methods could be established. This will allow for further studies of the molten chloride salt chemistry (e.g., corrosion) and development of the process technology for thermal energy storage systems up to 700 °C in the future.

REFERENCES

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